



# Getting the Most Out of Nafion<sup>TM</sup> Membranes

Clorosur Technical Seminar – Monterrey, Mexico  
15 November, 2018

# Agenda

- Overview
- Membrane Selection
- Membrane Protection
- Membrane Future Design
- Chemours Technical Service

# Overview

- Membrane chloralkali production plays a crucial and increasing role in today's chloralkali industry.
- All aspects of the membrane operational life cycle from selection to handling through operation are critical.
- This presentation will discuss the basics of the membrane life cycle with the primary emphasis on membrane protection during installation and operation.
- The future direction, and implications, of membranes will also be discussed.

# Membrane Selection



# Membrane Selection

Membrane selection is a complex, non-trivial process.

- What to consider:
  - Electrolyzer technology and its condition
  - Control scheme and operational capability
  - Operational parameters, target values and ranges
  - Brine quality, power costs, risk tolerance, etc.
- There are many parameters that need to be optimized for each customer and their priorities.

# Membrane Protection



# Membrane Protection

## Protect the membrane over its life cycle, during:

- Storage
- Handling while unpackaging, pre-treating and installing
- Operation
  - Initial startup
  - Routine startups, shutdowns, and operations
  - Load shedding
  - Emergency shutdowns

# Membrane Protection – Handling

Follow the membrane supplier's recommendations !

General guidelines:

- Ensure work areas are clean
- Ensure membrane contact surfaces are smooth, flat and free of debris, sharp edges and/or protrusions
- Membranes are fragile – avoid:
  - folding
  - kinking
  - dragging
  - pinching
  - impact damage
- Follow the recommended pre-treatment procedure for your membrane and situation



# Membrane Protection – Operational

Follow the technology supplier's and the membrane supplier's recommendations - discuss any conflicts with both suppliers !

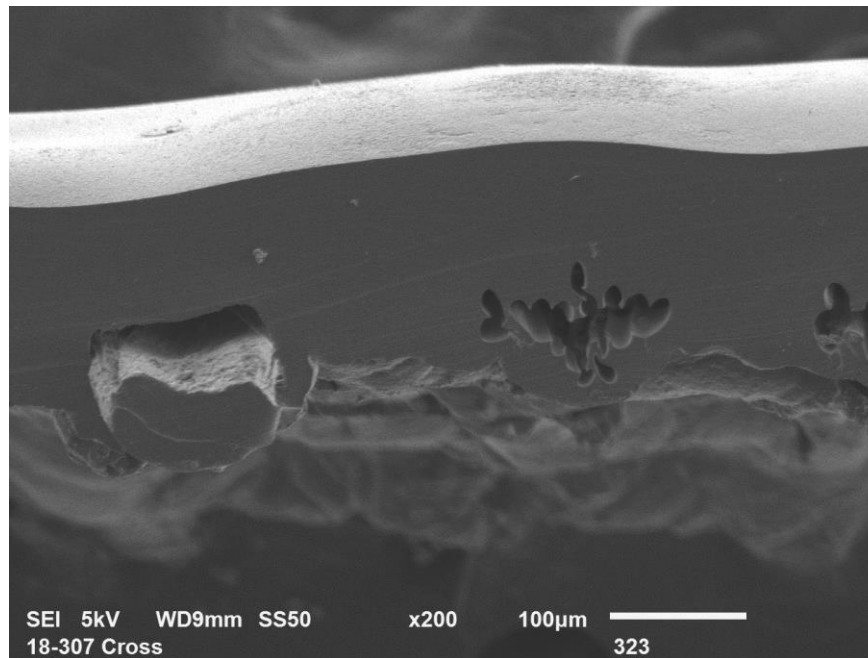
General guidelines for common items:

- Ensure that the electrolyte ionic (e.g. ~molar) strength is greater in the catholyte than the anolyte and that the catholyte level is maintained higher than the anolyte level at all times
- Avoid excessive differential pressures and/or differential pressure fluctuations, and avoid cold starts – the preferred startup temperature is  $\geq 70\text{ }^{\circ}\text{C}$  ( $\leq 85\text{ }^{\circ}\text{C}$ )
- Minimize brine impurities, don't just target "in-spec"
  - Simply put, cleaner brine = longer life

# Membrane Protection – Example

## Recent Analysis of N2030WX

- Continuously operated ~8.5 years at 5.5 kA/m<sup>2</sup>
- 96.5% current efficiency in post-mortem, laboratory test
- +10mV versus new membrane expectation



# Membrane Protection – Brine

## Sources of Impurities in Membrane Chloralkali Cells

1. **Salt** - multivalent cations, sulfate, silica, alumina, iodide, organics, etc.
2. **Water** - silica, multivalent cations, iodide, organics, etc.
3. **Hardware** - electrolyzer, piping, gaskets, instruments
4. **Process** - reaction generated & shutdown related

# Membrane Protection – Brine Impurity Effects

## Non-Organic Impurities

- Most non-organic impurities:
  - Damage the membrane by precipitating within or near its surfaces
  - Disrupt the polymer integrity resulting in current efficiency reduction
  - Plug ionic transport pathways resulting in voltage increase
  - Precipitates are most often in the form of hydroxide, iodide, sulfate and alumina salts (often complex salts)

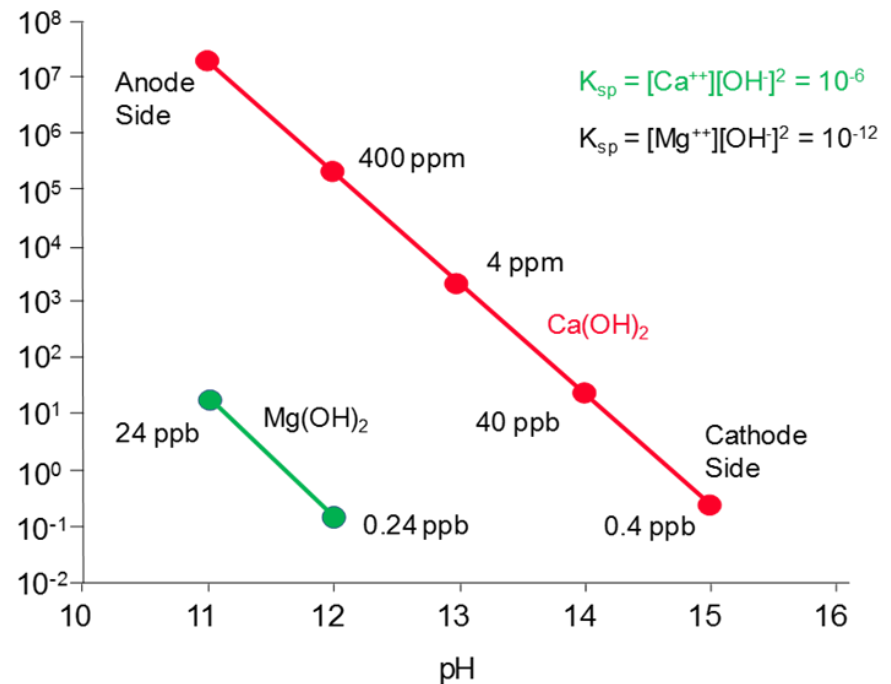
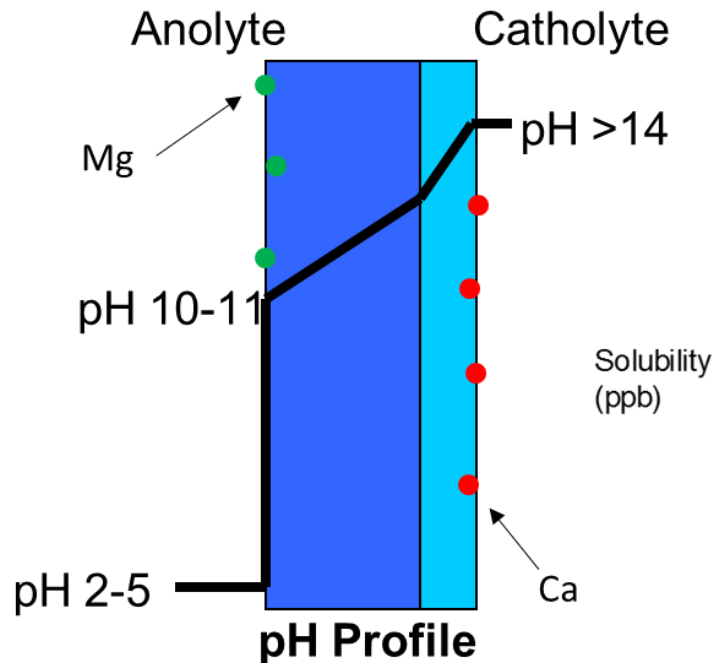
# Membrane Protection – Brine Impurity Effects

## Organic Impurities

- Organic impurities can:
  - Cause current efficiency reduction through polymer swelling
    - Polymer swelling effects may be reversed upon return to good brine feed or result in some permanent damage
  - Cause foaming at the top of the electrolyzer resulting in blistering damage to the membrane

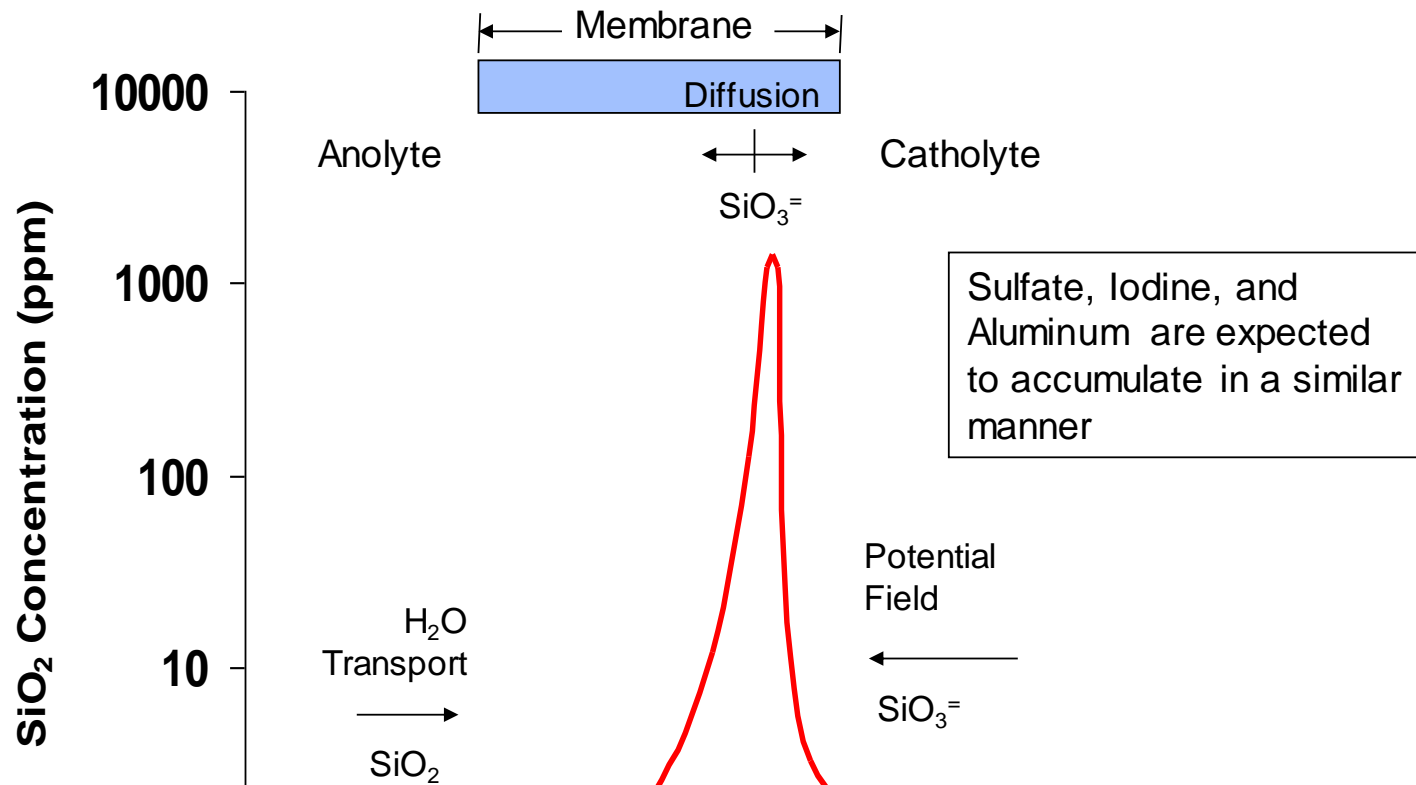
# Membrane Protection – Brine

## Magnesium and Calcium Precipitation in Membrane



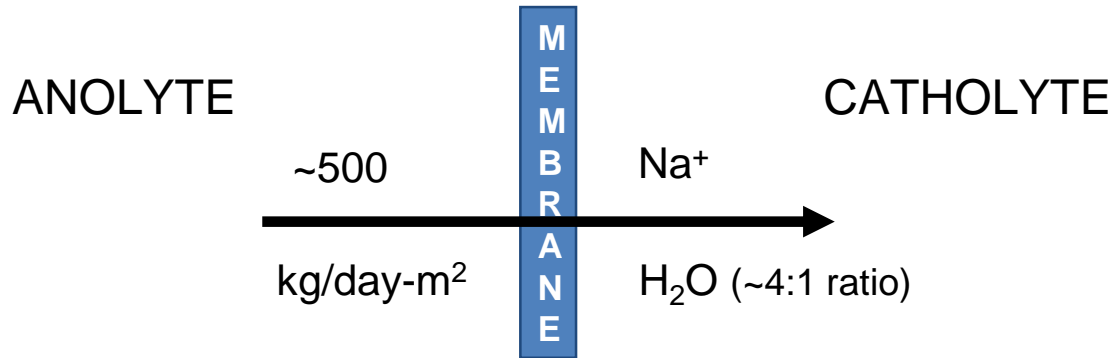
# Membrane Protection – Brine

## Predicted Silica Concentration Profile Across an Operating Membrane



# Membrane Protection – Brine

## Effect of 1 ppm Contaminant Membrane Mass Transport



Membrane weight ~ 350 g/m<sup>2</sup> (dry)  
6 kA/m<sup>2</sup>, 60 month life, 90% uptime

840,000 kg transported

$\times 10^{-6}$  (1 ppm wt/wt basis)

**840 g/m<sup>2</sup> Weight of Contaminant (100% deposited)**



# Membrane Protection – Brine

**Recommended Brine Impurity Limits for Chloralkali Plants Using Nafion™ Membranes**

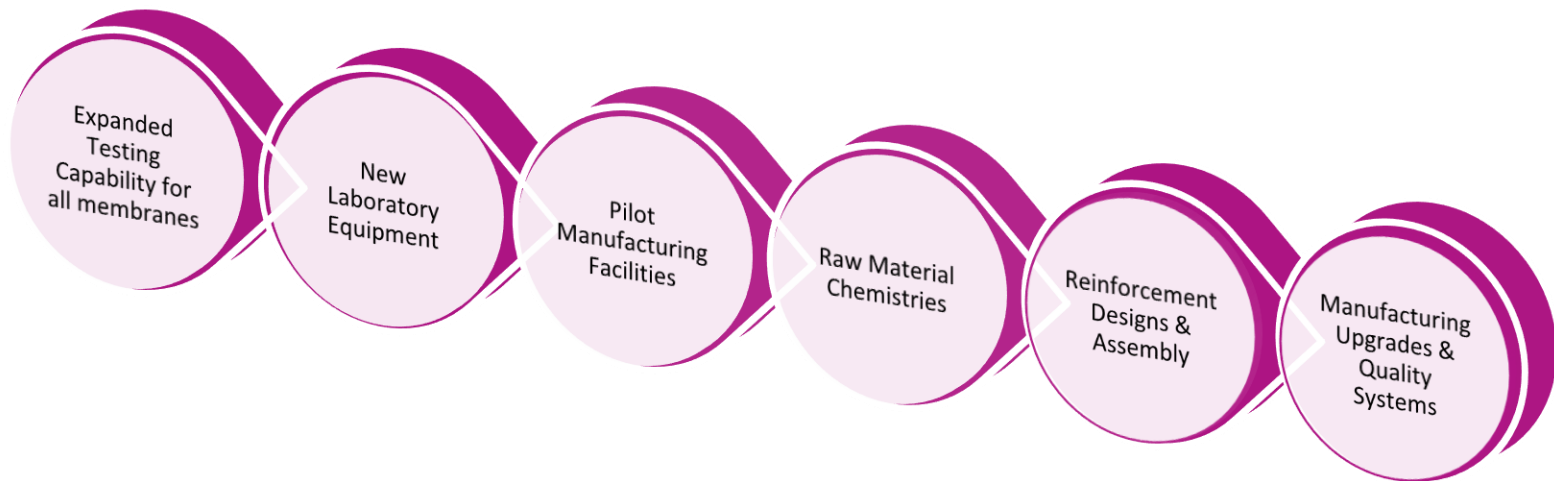
Impurity	Limit at 4 kA/m <sup>2</sup>	Limit at 4–6 kA/m <sup>2</sup>	Limit at 6–7 kA/m <sup>2</sup>	Primary Effect(s) on Performance if Limit Is Exceeded	Method(s) of Control (common)
Calcium and Magnesium (Ca + Mg)	<30 ppb (total)	<20 ppb (total)	<20 ppb (total)	Ca: Current efficiency (CE) decline. Mg: Voltage increase.	Ion exchange
Strontium (Sr)	<500 ppb	<400 ppb	<200 ppb	CE decline, small voltage increase.	Ion exchange
Barium (Ba)	<1.0 ppm	<500 ppb	<200 ppb	CE decline and voltage increase.	Ion exchange
Iodine (I)	<1.0 ppm	<200 ppb	<100 ppb	CE decline, possible voltage increase.	Purge of brine loop
Sodium Sulfate <sup>1</sup> (Na <sub>2</sub> SO <sub>4</sub> )	4–10 g/L	4–8 g/L	4–8 g/L	CE decline.	<ul style="list-style-type: none"> <li>• Primary treatment</li> <li>• Purge of brine loop</li> <li>• Filtration</li> <li>• Ion exchange</li> </ul>
Aluminum (Al)	<100 ppb	<100 ppb	<50 ppb	CE decline.	<ul style="list-style-type: none"> <li>• Primary treatment</li> <li>• Ion exchange</li> </ul>
Silica (SiO <sub>2</sub> )	<10 ppm	<6 ppm	<5 ppm	CE decline.	Primary treatment
Iron (Fe)	<1 ppm	<1 ppm	<100 ppb	None in moderate quantity. In large quantity, voltage can be elevated and permanent void damage can occur.	Monitor anti-caking agent content in raw salt
Total Organic Carbon (TOC)	<7 ppm	<7 ppm	<7 ppm	CE decline, increase in voltage, possible permanent membrane damage.	Elimination of source; filtration with activated carbon

<sup>1</sup>Minimum recommendation is to reduce effects of barium and iodide.

# Membrane Future Design

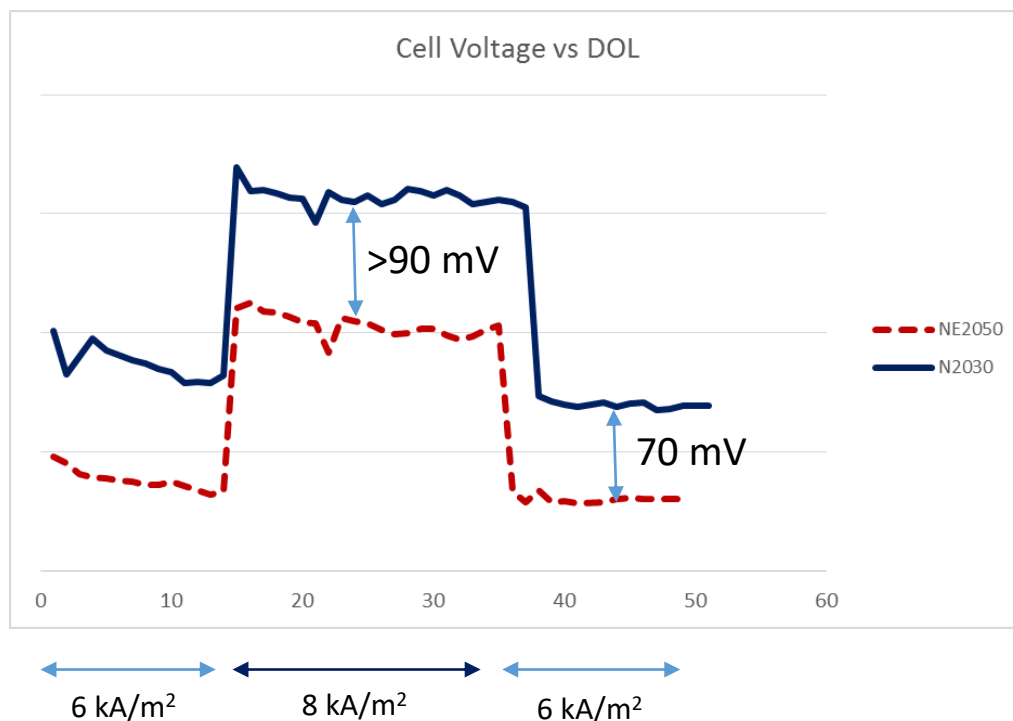


# Research & Technology: A Comprehensive Approach to Membrane Innovation



# Membrane Future – Chemours™ Test

## High Current Density Test



**N2050 membrane performs equivalent to N2030, with lower voltage and stable CE**

**SEM analysis after test shows no difference in membrane types. Membrane structure and CE stable**

Test Conditions  
Zero-gap cells, 100 cm<sup>2</sup>, 90°C








# Chemours Technical Service Team



# Chemours Technical Service Team

Our mission: Ensure Nafion™ membrane users get maximum value from our products

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Thank you